

Name:

Model-based Decision Support

Exam 6 (homework)

Enrolment number:

May, 2013

Blending and Combinatorial Optimization: The Hanford site in south-eastern Washington has produced nuclear materials using various processes for nearly 50 years. Radioactive hazardous waste was produced as by-products of the processes. This waste will be retrieved and separated into high-level and low-level portions. The high-level and low-level wastes will be immobilized for future disposal.

The high-level waste will be converted into a glass form for disposal. The glass must meet both processibility and durability restrictions. The processibility conditions ensure that during processing, the glass melt has properties within ranges known to be acceptable for the vitrification (glass-building) process. Durability restrictions ensure that the resultant glass meets the quantitative criteria for disposal in a repository. There are also bounds on the compositions of the various components in the glass. In the simplest case, waste and appropriate glass forms (frit) are mixed and heated in a melter to form a glass that satisfies the constraints. It is desirable to keep the amount of frit added to a minimum for two reasons. First, this keeps the amount of frit costs to a minimum. Second, the amount of waste per glass log formed is to be maximized, which keeps the waste disposal costs to a minimum. When there is only a single type of waste the problem of finding the minimum amount of frit is relatively easy (it is a blending problem).

However, Hanford has 21 Tanks (50K to 1M litres) containing radioactive waste. Because these wastes result from a variety of processes, these wastes vary widely in composition, and the glasses produced from these wastes will be limited by a variety of components. Table 1 shows an example of three tanks; especially it shows the chemical composition of the waste.

components / Tank ID	AZ-				W ^Λ
	AY-102	101	AZ-102		
SiO ₂ (silicon dioxide)	1	0,072	0,092	0,022	11,18365
B ₂ O ₃ (boron oxide)	2	0,026	0	0,006	2,416554
Na ₂ O	3	0,105	0,264	0,12	34,19368
Li ₂ O	4	0	0	0	0
CaO (quicklime)	5	0,061	0,012	0,01	5,56847
MgO	6	0,04	0	0,003	2,822121
Fe ₂ O ₃	7	0,328	0,323	0,392	89,00615
Al ₂ O ₃	8	0,148	0,157	0,212	45,66483
ZrO ₂	9	0,002	0,057	0,063	11,47892
Other	10	0,217	0,096	0,173	41,71802
Total		0,999	1,001	1,001	244,0524
Cr ₂ O ₃	11	0,016	0,007	0,005	1,95795
F	12	0,006	0,001	0,001	0,542788
P ₂ O ₃	13	0,042	0,001	0,021	5,56952
SO ₃	14	0,001	0,018	0,009	2,080857
Noble Metals	15	0	0	0	0
Mass (unit tons)		59,772	40,409	143,747	243,928

Table 1

Table 1 shows the waste mass expressed as a total of the first ten chemicals, including the “chemical” termed as “Other.” The waste mass is scaled down by 1000, let say the units are tons. In the table the chemicals are expressed as the fraction of the total mass of the corresponding tank (tanks are labelled AY-102, AZ-101 etc.). The full information for all 21 Tanks you’ll find in an extra GAMS file. Additionally it should be mentioned that the substances Cr₂O₃, F, P₂O₃, SO₃, and Noble Metals are known components of Other: these substances represent only a small amount of Other but have a huge

impact on the vitrification process. Other substances of Other (like water) are uncritical. Note that Cr2O3, Flour (F) etc. are no extra components but are aggregated in Other.

Frit added to a blend of tanks consists of the first nine chemicals or something else like water (the latter one are formally added to Other frit). Of course, the frit Other is not polluted by Cr2O3, F, etc. The minimum amount of frit would be used if all the high-level wastes were combined to form a single feed to the vitrification process. Because of the volume of waste involved and the time span over which it will be processed, this is logistically impossible. However, much of the same benefit can be obtained by forming blends from sets of tanks.

The problem is how to divide all the 21 tanks into sets to be blended together so that a minimum amount of frit is required. Let us assume that the 21 tanks should be combined of three groups each with 7 tanks. One decision is to group the tanks (combinatorial problem). The other decisions (for each group of tanks separately done) are the fractions of i^{th} component in the glass (different for each group of tanks), i.e. p_i $i = \text{SiO}_2, \text{B}_2\text{O}_3$ etc. (blending problems).

Additionally you have some auxiliary decisions variables for “amount of component i originally in the blend (group of tanks) $W^{(i)}$ ”, “mass of the i^{th} component in the frit ($f^{(i)}$)”, “mass of i^{th} component in the glass (blend) $g^{(i)}$ ” and the total mass of the blend G . It should be obvious that $W^{(i)}$ is computed with data like in Table 1, $f^{(i)}$ relates to $p^{(i)}$ via G ($p = f/G$), $g^{(i)}$ results from the sum of $f^{(i)}$ and $W^{(i)}$, G is the sum of the $g^{(i)}$ (of course done for every group of tanks).

In order to form glass, a blend must satisfy certain constraints:

Details of Glass Property Constraints

NOTATION

C_1	Bound for Crystal1 – 3.0
C_2	Bound for Crystal2 – 0.08
C_3	Bound for Crystal3 – 0.225
C_4	Bound for Crystal4 – 0.18
C_5	Bound for Crystal5 – 0.18
k_{\min}	Lower limit for conductivity – 18
k_{\max}	Upper limit for conductivity – 50
μ_{\min}	Lower limit for viscosity (PaS) – 2.0
μ_{\max}	Upper limit for viscosity (PaS) – 10.0
D_{\max}^{PCT}	Max release rate (product consistency test) (g per m_2) – 10.0
D_{\max}^{MCC}	Max release rate (materials characterization center) (g per m^2) – 28.0
μ_a^i	Linear coefficients of viscosity model
μ_b^{ij}	Cross term coefficients of viscosity model
k_a^i	Linear coefficients of electrical conductivity model
k_b^{ij}	Cross term coefficients of electrical conductivity model
Dp_a^i	Linear coefficients of durability (PCT) model (for Boron)
Dp_b^{ij}	Cross term coefficients of durability (PCT) model for Boron
Dm_a^i	Linear coefficients of durability (MCC) model (for Boron)
Dm_b^{ij}	Cross term coefficients of durability (MCC) model (for Boron)

1. Component Bounds:

- $0.42 \leq p^{(\text{SiO}_2)} \leq 0.57$
- $0.05 \leq p^{(\text{B}_2\text{O}_3)} \leq 0.20$
- $0.05 \leq p^{(\text{Na}_2\text{O})} \leq 0.20$
- $0.01 \leq p^{(\text{Li}_2\text{O})} \leq 0.07$
- $0.0 \leq p^{(\text{CaO})} \leq 0.10$
- $0.0 \leq p^{(\text{MgO})} \leq 0.08$

- g) $0.02 \leq p^{(\text{Fe}_2\text{O}_3)} \leq 0.15$
- h) $0.0 \leq p^{(\text{Al}_2\text{O}_3)} \leq 0.15$
- i) $0.0 \leq p^{(\text{ZrO}_2)} \leq 0.13$
- j) $0.01 \leq p^{(\text{other})} \leq 0.10$

2. Five glass crystallinity constraints:

- a) $p^{(\text{SiO}_2)} > p^{(\text{Al}_2\text{O}_3)} * C_1$
- b) $p^{(\text{MgO})} + p^{(\text{CaO})} < C_2$
- c) $p^{(\text{Fe}_2\text{O}_3)} + p^{(\text{Al}_2\text{O}_3)} + p^{(\text{ZrO}_2)} + p^{(\text{Other}')} < C_3$
- d) $p^{(\text{Al}_2\text{O}_3)} + p^{(\text{ZrO}_2)} < C_4$
- e) $p^{(\text{MgO})} + p^{(\text{CaO})} + p^{(\text{ZrO}_2)} < C_5$

3. Solubility Constraints:

- a) $p^{(\text{Cr}_2\text{O}_3)} < 0.005$
- b) $p^{(\text{F})} < 0.017$
- c) $p^{(\text{P}_2\text{O}_5)} < 0.01$
- d) $p^{(\text{SO}_3)} < 0.005$
- e) $p^{(\text{Rh}_2\text{O}_3 + \text{PdO} + \text{Ru}_2\text{O}_3)} < 0.025$

4. Viscosity Constraints:

- a) $\sum_{i=1}^n \mu_a^i * p^{(i)} + \sum_{j=1}^n \sum_{i=1}^n \mu_b^{ij} * p^{(i)} * p^{(j)} > \log(\mu_{\min})$
- b) $\sum_{i=1}^n \mu_a^i * p^{(i)} + \sum_{j=1}^n \sum_{i=1}^n \mu_b^{ij} * p^{(i)} * p^{(j)} < \log(\mu_{\max})$

5. Conductivity Constraints:

- a) $\sum_{i=1}^n k_a^i * p^{(i)} + \sum_{j=1}^n \sum_{i=1}^n k_b^{ij} * p^{(i)} * p^{(j)} > \log(k_{\min})$
- b) $\sum_{i=1}^n k_a^i * p^{(i)} + \sum_{j=1}^n \sum_{i=1}^n k_b^{ij} * p^{(i)} * p^{(j)} < \log(k_{\max})$

6. Dissolution rate for boron by PCT test (DissPCTbor):

$$\sum_{i=1}^n Dp_a^i * p^i + \sum_{j=1}^n \sum_{i=1}^n Dp_b^{ij} * p^{(i)} * p^{(j)} < \log(D_{\max}^{\text{PCT}})$$

7. Dissolution rate for boron by MCC test (DissMCCbor):

$$\sum_{i=1}^n Dm_a^i * p^i + \sum_{j=1}^n \sum_{i=1}^n Dm_b^{ij} * p^{(i)} * p^{(j)} < \log(D_{\max}^{\text{MCC}})$$

I'll provide a GAMS file at TISS where the declaration part and the coded model are already provided. Solve this problem using a Mathematical Programming solver (keep in mind that due to the size of the problem a single optimization run may last a little bit longer) and describe the results partly in tables and partly verbally. Please add the name of the solver that you have used and how long the computation has lasted (in minutes).

Next add constraints that the total mass of a group of tanks (waste plus frits) is not twice as much as the mass of any of the two other groups of tanks. Report the results of this extended problem.

You can discuss this homework with your colleagues but please do this homework separately. The deadline for this homework is May 16th, 2013.

I hope I don't frustrate you by the following link (luckily in Austria we don't have such problems):

<http://www.komonews.com/news/local/Tank-leaking-radioactive-waste-at-Hanford-191454201.html>